Photocatalytic degradation of the herbicide clopyralid: kinetics, degradation pathways and ecotoxicity evaluation

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Abstract

BACKGROUND: Photocatalytic decomposition and mineralization of the herbicide clopyralid in aqueous solutions has been studied, aiming at an extended kinetic analysis, the elucidation of potential degradation pathways and the determination of ecotoxicity.

RESULTS: The pseudo-first-order degradation kinetics was studied under different operational conditions, such as type of photocatalyst, catalyst loading, initial pH and hydrogen peroxide (H₂O₂) concentration. The degradation rates proved to be strongly influenced by these parameters. Organic chlorine and nitrogen were easily converted into inorganic in the presence of TiO₂ P25, resulting in 90% conversion in both cases within 180 min of illumination, while conversion was enhanced in the presence of H₂O₂. Ten possible transformation products were identified by means of LC-DAD-ESI/MS analysis. Acute toxicity profiles using marine bacteria Vibrio fischeri showed an increasing trend during the first 60 min of illumination, which thereafter, progressively decreased.

CONCLUSIONS: Intermediates were formed mainly through pyridine ring transformation, dechlorination and decarboxylation reactions. The increasing trend in ecotoxicity at the first stages of degradation could be attributed to the progressive formation of intermediates more toxic than the parent molecule, or due to synergistic effects among the transformation products.

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Keywords: clopyralid; pesticide; photocatalytic; TiO₂; toxicity; intermediates

INTRODUCTION

Introduction of synthetic organic chemicals in agricultural processes during the second half of the twentieth century not only boosted the ability to counter crop-spoiling organisms, but also enabled the control of parasite-borne health and life-threatening diseases (i.e. malaria), improving the quality of life of large populations and allowing better utilization of agricultural areas. However, the widespread use of pesticides has led to widespread contamination of the environment with these bio-recalcitrant organic compounds.1,2 In highly industrialized countries the problem of pesticide wastes is mainly related to wastewater, recycling, elimination of packaging (containers, etc.) after use and the remediation of contaminated soils. For developing countries, the main problem is the elimination of unused (forbidden), obsolete and unusable pesticide stocks.3 The United Nations estimates that less than 1% of all pesticides used in agriculture actually reaches the crops. The remainder contaminates the land, the air and particularly the water. These xenobiotics are in many cases toxic and non-biodegradable, with the potential to cause adverse acute or chronic toxic health effects to non-target organisms4 and to accumulate in the environment through the global trophic network with unpredictable consequences.5–6

Clopyralid (3,6-dichloro-2-pyridine-carboxylic acid) is a systemic herbicide from the chemical class of pyridine compounds, often detected in drinking water.7 It is used to control annual and perennial broadleaf weeds in certain crops and turf and provides control of some brush species on rangeland and pastures. Clopyralid may be persistent in soil under anaerobic conditions and with low microorganism content, with half-life ranging from 15 to more than 280 days.8 It presents high solubility in water and is particularly stable against hydrolysis and photolysis. Its chemical stability, along with its mobility, enables this herbicide to penetrate through soil, causing long term contamination of ground and surface water supplies8,9 along with losses in production of certain plant species.
Photocatalytic degradation of clopyralid: kinetics, degradation pathways and ecotoxicity

Heterogeneous photocatalytic oxidation (TiO$_2$/UV-A) has been proven to be effective for the degradation of a variety of toxic agrochemical substances, such as insecticides and pesticides, in the presence of artificial or solar illumination, while studies dealing with real or simulated wastewater have revealed that their complete or partial degradation is possible via the above mentioned methods. Previous studies have published data on the photocatalytic degradation of clopyralid employing for the first time a wide range of commercial photocatalysts, providing a thorough kinetic analysis in terms of degradation and mineralization. New intermediates have been identified and detailed degradation pathways have been proposed. Furthermore, for the first time we provide data on the reduction of marine bacteria in aqueous solutions of clopyralid treated with TiO$_2$, P25. The present study is implemented within the framework of a research project aiming at the development of a combined system for the detoxification and reuse of wastewater containing pesticides by solar photocatalysis and constructed wetlands.

MATERIALS AND METHODS

Materials

Clopyralid (3,6-dichloro-2-pyridine-carboxylic acid, CAS No. 1702-17-6, $M_r$: 192 g mol$^{-1}$, Product No: 3675B, Pestanal, analytical standard) was a product of Fluka (Sigma–Aldrich Labchemici cal GmbH) and was used as received.

The catalysts used were TiO$_2$ P25 (Degussa Evonik GmbH, anatase/rutile = 3:6/1, Brunauer-Emmett-Teller (BET) surface area: 50 m$^2$ g$^{-1}$, nonporous), TiO$_2$ UV-100 (Hombikat, 100% anatase, BET: 300 m$^2$ g$^{-1}$), TiO$_2$ Kronos (7000, 7001, 7500, Kronos Worldwide, Inc, 100% anatase, BET: 250 m$^2$ g$^{-1}$) and ZnO (Merck, BET: 10 m$^2$ g$^{-1}$). All other reagent-grade chemicals were purchased from Merck and were used without further purification. Doubly deionized water was used throughout the study.

Photocatalytic experiments

Experiments were performed in a closed Pyrex cell of 600 mL capacity, fitted with a central 9 W lamp, under magnetic stirring. The cell had inlet and outlet ports for bubbling CO$_2$ free air during photocatalysis. The spectral response of the irradiation source (Osmar Dulux S, 9 W/78) ranged between 350 and 400 nm with a maximum at 366 nm. The incident photon flow of the irradiation source, determined by chemical actinometry using potassium ferrioxalate, was 97 × 10$^{-6}$ Einstein L$^{-1}$ min$^{-1}$.

Photocatalysis was conducted at a working volume of 500 mL, at 4.7 ± 0.1 initial pH and constant temperature (25 ± 0.1 °C). Maximum dark adsorption of clopyralid onto the semiconductor surface was achieved within 30 min. At specific time intervals samples of 6 mL were taken and filtered through a 0.45 μm filter (Schleicher and Schuell).

Analytical procedures

Changes in the concentration of clopyralid were monitored via its characteristic absorption band at 280 nm using a UV-Visible spectrophotometer (UV-1700, PharmaSpec, Shimadzu). Since a linear dependence between the initial concentration of the pesticide and the absorption at 280 nm is observed, the photodecomposition was monitored spectrophotometrically at this wavelength.

Determination of dissolved organic carbon (DOC) was conducted according to standard methods by a total organic carbon (TOC) analyser (Shimadzu V$_{CSH}$ 5000).

Inorganic ions were determined in a Shimadzu system consisting of a LC-10 AD pump, a CDD-6A conductometric detector (0.25 μL flow-cell) and a CTO-10A column oven. Cations were separated on an Alltech Universal column (100 mm × 4.6 mm) preceded by a guard column (7.5 mm × 4.6 mm) of the same material using 3 mmol L$^{-1}$ methanesulfonic acid at 1.5 mL min$^{-1}$ constant flow. Anions were separated on an Alltech Allsep column (100 mm × 4.6 mm) preceded by a guard column (7.5 mm × 4.6 mm) of the same material using a phthalic acid and lithium hydroxide mixture of 4 mmol L$^{-1}$ (pH 4.00) at 1.5 mL min$^{-1}$ constant flow. Column and conductivity cell temperatures were held constant at 35 °C and 38 °C, respectively. Mobile phases were degassed with helium stream prior to liquid chromatography (LC). Calibration curves (0.01–10 mg L$^{-1}$) were constructed for each ion.

Some photocatalytic experiments were repeated three times to check the reproducibility of the experimental results. The accuracy of the optical density values was within ±5%, while in the case of DOC and inorganic ions analysis it was ±10%.

Liquid chromatography, with diode array detection and electrospray ionisation mass spectrometry (LC DAD ESI/MS) was conducted as follows: the HPLC system consisted of a SIL 20A autosampler and a LC-20AB pump, both from Shimadzu (Kyoto, Japan). The analytes were separated using a C$_{18}$ analytical column of 150 × 4.6 mm with 5 μm particle size (Restek, USA). Detection was carried out using a SPD 20A DAD detector coupled in series with the LC-MS 2010EV mass selective detector, equipped with an atmospheric pressure electrospray ionization (ESI) source. The samples were analysed using the ESI interface in positive ionization (PI) mode. For the analysis in PI mode a gradient elution was performed by a binary gradient, composed of solvent A (water/0.1% HCOOH) and solvent B (methanol/0.1% HCOOH) according to the following program: initial conditions 80% A, kept constant for 1 min, decreased to 50% in 4 min, decreased to 10% in 50 min, kept constant for 6 min, returned to the initial conditions after 2 min. Re-equilibration time was set at 2 min, while the total run analysis lasted 60 min. Column temperature was set at 40 °C and the flow rate was 0.2 mL min$^{-1}$. The drying gas was operated at 10 L min$^{-1}$ flow at 200 °C. The nebulizing pressure was 100 psi, capillary voltage was 4500 V and the fragmentation voltage was set at 5 V (for PI ionization).

Quality assurance and quality control for LC-DAD-ESI/MS analysis

Identification and confirmation of clopyralid in water samples was made by comparing the retention time, identifying the target and qualifier ions and determining the qualifier-to-target ratios of the peak in the samples with that of a pesticide standard. Acceptance criteria for positive identification consisted of retention times within 0.20 min of the expected value and % qualifier-to-target ratios within 30% of the standard (10 mg L$^{-1}$).

Internal quality control was applied in every batch of samples in order to check if the system is under control. A quality control sample (10 mg L$^{-1}$ standard) was run every five injections, followed by a blank sample (pure methanol). Nine gradients of standard solutions (0.1, 0.5, 1, 5, 10, 25, 50, 75, 100 mg L$^{-1}$) were adopted. To avoid the impact of linearity issues on quantification accuracy, the target compound concentrations always fall within the middle
range of the standard curve. Calibration curves for the analyte were drawn with five points and the determination coefficients \((R^2)\) of the regression curves were >0.993.

Precision of the LC-MS chromatographic method, determined as relative standard deviation (RSD), was obtained from repeated injections \((n=5)\) of a sample during the same day (repeatability) and in different days (reproducibility). In all cases RSD\% values <10\% were obtained.

Limit of detection (LOD) and limit of quantification (LOQ) were defined to be the lowest observable concentration of analyte in spiked water samples giving a signal to noise \((S/N)\) ratio of 3 and 10, respectively. LOD and LOQ values were 0.020 mg L\(^{-1}\) and 0.060 mg L\(^{-1}\), respectively.

### Toxicity analysis

Bioluminescence ecotoxicity test using marine bacteria Vibrio fischeri was applied to provide information on acute toxicity of the intermediates formed during photocatalysis. The osmolality of the samples was adjusted by 2\% w/v NaCl, while pH was adjusted between 6.5 and 8.5. Toxicity was evaluated using the Microtox Model 500 Analyzer (Azur Environmental). Freeze-dried bacteria, reconstitution solution, diluent (2\% w/v NaCl) and adjustment solution (non-toxic 22\% w/v NaCl) were obtained from Azur. Samples were tested in a medium containing 2\% w/v NaCl, in five dilutions and luminescence was recorded after 5, 15 and 30 min incubation. The inhibition of bioluminescence, compared with a toxic-free control to give the percentage of inhibition, was calculated using the Microtox calculation software.

### RESULTS AND DISCUSSION

#### Heterogenous photocatalytic experiments

Results of the degradation of a 40 mg L\(^{-1}\) clopyralid solution containing 0.5 g L\(^{-1}\) TiO\(_2\) P25, TiO\(_2\) UV-100, ZnO, TiO\(_2\) Kronos 7000, Kronos 7001 and Kronos 7500 under UV-A irradiation are shown in Fig. 1 while the respective initial degradation rates are presented in Table 1. The concentration of clopyralid is plotted as a function of the irradiation time. Under the given experimental conditions, ZnO and TiO\(_2\) P25 in the presence of UV-A appear to be the best catalysts resulting after 180 min of illumination in 95 and 75\% degradation of the pesticide, respectively. Although ZnO has similar band gap energy and band edge positions to TiO\(_2\), its photocatalytic efficiency of P25 among various grades of TiO\(_2\). In the case of TiO\(_2\) P25 a transfer of the photogenerated electrons from rutile to anatase particles takes place, leading to stabilization of charge separation and therefore, limits the recombination of the photogenerated carriers. In addition, the small size of rutile particles in this formulation and their close proximity to anatase particles are crucial to enhance the catalyst activity.

The effect of the initial equilibrium concentration of clopyralid on the initial reaction rate \((r_0)\) of photodecomposition is shown in Fig. 2. The \(r_0\) values were independently obtained by a linear fit of the \(C−t\) data in the range 5–50 mg L\(^{-1}\) of initial clopyralid concentration. The curve is reminiscent of a Langmuir type isotherm, for which the rate value of photodecomposition first increases and then reaches a saturation value at higher concentrations of clopyralid.

The influence of the initial concentration of an organic compound on the photocatalytic degradation rate of most organic compounds is described by a pseudo-first-order kinetics, which is rationalized in terms of the Langmuir–Hinshelwood model, modified to be valid for reactions occurring at a solid–liquid interface:

\[
r_0 = -\frac{dC}{dt} = \frac{k_rKC}{1 + KC}
\]

where \(r_0\) is the initial degradation rate and \(C\) is the concentration of the organic substrate. \(K\) represents the equilibrium constant

Table 1. Initial rates of photodegradation \((r_0)\) of 40 mg L\(^{-1}\) clopyralid in the presence of 0.5 g L\(^{-1}\) of various photocatalysts

<table>
<thead>
<tr>
<th>Conditions</th>
<th>(r_0) (mg L(^{-1}) min(^{-1})) ± standard error</th>
</tr>
</thead>
<tbody>
<tr>
<td>TiO(_2) P25</td>
<td>0.228 ± 0.009</td>
</tr>
<tr>
<td>ZnO</td>
<td>0.828 ± 0.056</td>
</tr>
<tr>
<td>TiO(_2) UV 100</td>
<td>0.160 ± 0.018</td>
</tr>
<tr>
<td>TiO(_2) Kronos 7000</td>
<td>0.075 ± 0.004</td>
</tr>
<tr>
<td>TiO(_2) Kronos 7001</td>
<td>0.087 ± 0.004</td>
</tr>
<tr>
<td>TiO(_2) Kronos 7500</td>
<td>0.086 ± 0.009</td>
</tr>
</tbody>
</table>

Figure 1. Photocatalytic degradation of 40 mg L\(^{-1}\) of clopyralid in the presence of various commercial catalysts at an initial concentration of 0.5 g L\(^{-1}\) and UV-A irradiation: (■) TiO\(_2\) P25, (●) ZnO, (▲) TiO\(_2\) UV-100 (▼) TiO\(_2\) Kronos 7000, (●) TiO\(_2\) Kronos 7001, (▲) TiO\(_2\) Kronos 7500. Error: 5%.

On the other hand, the efficiency of the other commercial forms of TiO\(_2\) in the oxidation of clopyralid under UV-A irradiation is a considerably slower process and decreases in the order: TiO\(_2\) UV-100 < TiO\(_2\) Kronos 7500 < TiO\(_2\) Kronos 7001 < TiO\(_2\) Kronos 7000, with TiO\(_2\) UV-100 resulting in 62\% degradation after 180 min of illumination (Fig. 1). The superiority of TiO\(_2\) P25 may be attributed to the morphology of its crystallites, which has been proposed as one of the most critical properties for the photocatalytic efficiency of P25 among various grades of TiO\(_2\).
The $r$ and $K$ values calculated according to Equation (2) from the above $0.25 \text{gL}^{-1}$ increase of the initial mineralization rate at concentrations a saturation value at higher TiO$_2$ concentrations. In this study, the optimum value for TiO$_2$ P25 is $1.0 \text{gL}^{-1}$. The pH value, on the other hand, plays an important role in the adsorption of the organic substrate onto the semiconductor and $K_r$ reflects the limiting rate constant of reaction at maximum coverage under the given experimental conditions. This equation can be used when data demonstrate linearity plotted as follows:

$$\frac{C}{r_0} = \frac{1}{k_rK} + \frac{C}{k_r} \tag{2}$$

As indicated in the inset of Fig. 2 the plot of the reciprocal initial rate, $r_0$, as a function of the initial concentration, $C$, yields for constant concentration of TiO$_2$ P25 at $0.5 \text{gL}^{-1}$ a straight line. The $k_r$ and $K$ values calculated according to Equation (2) from the slope and the intercept with the $1/r_0$ axis of the resulting straight line ($R^2 = 0.98$), were $0.28 \pm 0.01 \text{mg L}^{-1} \text{min}^{-1}$ (1.46 $10^{-6} \pm 0.05$ $10^{-9} \text{mol L}^{-1} \text{min}^{-1}$) and $0.15 \pm 0.03 \text{mg L}^{-1}$ (0.78 $\pm 0.16 \text{L mol}^{-1}$), respectively.

TiO$_2$ dosage in slurry photocatalytic processes is an important factor that can strongly influence the degradation of the organic compound. The optimum quantity depends on the nature of the organic compound, as well as on the photoreactor’s geometry. The values of the initial degradation rate in relation to the catalyst dose follow a Langmuir type isotherm, suggesting that $r_0$ might reach a saturation value at higher TiO$_2$ concentrations. In this study, the optimum value for TiO$_2$ P25 is $1.0 \text{gL}^{-1}$, while further increase in the amount of TiO$_2$ leads to a slight decrease in the efficiency of photodegradation (Fig. 3). This limit depends on the geometry and the working conditions of the reactor and corresponds to the optimum of light absorption. Above this optimum concentration, the suspended particles of the catalysts block the UV-light passage and increase the light scattering. Furthermore, the decrease of the reaction rate at high catalyst concentrations is due to other phenomena such as agglomeration (particle–particle interactions), resulting in a loss of surface area available for light-harvesting. On the contrary, the increase of TiO$_2$ P25 loading leads to no further increase of the initial mineralization rate at concentrations above $0.25 \text{gL}^{-1}$ (Fig. 3).

The pH value, on the other hand, plays an important role in the photocatalytic degradation of various organic pollutants. Some properties of the photocatalyst, such as surface charge state and flat band potential are highly pH dependent, while electrostatic attraction or repulsion between the catalyst’s surface and the organic molecule, depending on the ionic form of the organic compound (anionic or cationic) enhances or inhibits, respectively, the photodegradation rate. Moreover, pH influences the size of TiO$_2$ aggregates, the interaction of the solvent molecules with the catalyst and the type of radicals or intermediates formed during the photocatalytic process. All of these factors have a significant influence on the adsorption of organic molecules onto TiO$_2$ and affect the observed removal rates. The effect of pH on clopyralid initial degradation and mineralization rates during heterogeneous photocatalytic oxidation of $40 \text{gL}^{-1}$ of clopyralid in the presence of $0.5 \text{gL}^{-1}$ TiO$_2$ P25 and UV-A irradiation: $r_0$ ($\bullet$) $r_{DOC}$.}

![Figure 2. Plot of $r_0$ vs $C$ at various initial concentrations of clopyralid from 5 to $50 \text{gL}^{-1}$ for constant concentration of TiO$_2$ P25 at $0.5 \text{gL}^{-1}$. Inset: linear transformation of $C/r_0$ vs $C$ according to Equation (2).]

![Figure 3. Effect of the TiO$_2$ P25 concentration on initial ($\bullet$) degradation ($r_0$) and ($\bullet$) mineralization ($r_{DOC}$) rates of clopyralid, during heterogeneous photocatalysis under UV-A irradiation for $40 \text{gL}^{-1}$ of the pesticide.]

![Figure 4. Effect of pH on clopyralid initial degradation and mineralization during heterogeneous photocatalytic oxidation of $40 \text{gL}^{-1}$ of clopyralid in the presence of $0.5 \text{gL}^{-1}$ TiO$_2$ P25 and UV-A irradiation: $r_0$ ($\bullet$) $r_{DOC}$.]
than 6.35, favorable for attracting anions, and TiO₂ deprotonates in solutions with a pH higher than 6.35, hence its surface becomes negatively charged (TiO²⁻), favorable for repelling anions. At pH 3.0, clopyralid ionizes significantly to cations and the surface charges of TiO₂ are predominantly positive (pH < pzcTiO₂). This creates an unfavorable condition for attracting clopyralid to the surface of TiO₂, resulting in low degradation rates. As pH increases from 3.0 to 4.7, clopyralid becomes less positively charged and at pH 4.7 is even negatively charged, yet TiO₂ surface is still positively charged, favorable for attraction of the two species and for high degradation and mineralization rates (Fig. 4). A further increase of pH, in particular beyond pzcTiO₂ (6.35), results in accumulation of negative charges on the surface of TiO₂, causing repulsion of the negatively charged clopyralid molecules. Thus, surface adsorption and initial degradation and mineralization rates decrease. Similar results on the effect of pH on the initial degradation rate of clopyralid were reported by C. Tizaoui et al. The addition of species with the potential to capture the photogenerated electrons, such as hydrogen peroxide and potassium peroxydisulfate, to TiO₂/UV-A suspensions is an extensively studied procedure often leading to an acceleration of the photocatalytic degradation rate. In our case the photocatalytic oxidation of 40 mg L⁻¹ of clopyralid in the presence of 0.5 g L⁻¹ TiO₂ P-25 has been studied at different initial H₂O₂ concentrations (Fig. 5). The reaction kinetics were similar to those observed upon prolonged irradiation, were oxidized to NO₃⁻, while only trace amounts of NO₂⁻ were detected which, upon prolonged irradiation, were oxidized to NO₃⁻. Nitrogen conversion is more effective in the presence of TiO₂ P-25 compared with TiO₂ UV-100 (almost 80% and 30% conversion rates, respectively, after 180 min of illumination), while in both cases the activity of the catalysts is enhanced in the presence of H₂O₂.

Degradation by-products and reaction pathways
Photocatalytic mineralization of clopyralid proceeds through the formation of various reaction intermediates, whose carbon atoms are eventually converted to carbon dioxide, while heteroatoms are converted to inorganic ions that remain in the liquid phase. Clopyralid mineralization can be described by the following overall reaction scheme:

\[
\text{C}_6\text{H}_3\text{O}_2\text{NCl}_2 + \frac{13}{2}\text{O}_2 \rightarrow 6\text{CO}_2 + \text{HNO}_3 + 2\text{HCl}
\]  (3)

To elucidate the routes through which clopyralid is converted to reaction by-products and eventually to end-products, besides the DOC reduction (Figs 3 and 4), samples were analyzed with respect to: (i) the release of inorganic chlorine and nitrogen species in the reaction mixture; and (ii) the identification of major intermediates. Figures 6 and 7 show temporal profiles of chloride anions and total inorganic nitrogen (i.e. contained in nitrates, nitrites and ammonium ions), respectively, released during the photocatalytic oxidation of clopyralid. Profiles do not show actual concentrations but they correspond to the percentage of the theoretical amount of chloride or nitrogen initially present in the clopyralid molecule. Organic chlorine is easily converted into inorganic in the presence of TiO₂ P-25 (almost 87% conversion within 180 min of illumination, Fig. 6). TiO₂ UV-100, under the same experimental conditions, leads to 35% conversion of chlorine, while in both cases the photocatalyst’s activity is enhanced in the presence of H₂O₂.

Similar results are obtained regarding the conversion of nitrogen of the pyridine ring of clopyralid in NO₃⁻ and NH₄⁺. Figure 7 shows concentration–time profiles of total inorganic nitrogen (i.e. the sum of nitrogen contained in NO₃⁻, NH₄⁺ and NO₂⁻) as a percentage of the theoretical nitrogen in clopyralid, under various experimental conditions. In all cases, ammonium and nitrate were the dominant inorganic species formed during photocatalytic degradation, while only trace amounts of NO₂⁻ were detected which, upon prolonged irradiation, were oxidized to NO₃⁻. Nitrogen conversion is more effective in the presence of TiO₂ P-25 compared with TiO₂ UV-100 (almost 80% and 30% conversion rates, respectively, after 180 min of illumination), while in both cases the activity of the catalysts is enhanced in the presence of H₂O₂.

The transformation mechanism of clopyralid during the photocatalytic process was investigated. Ten (10) transformation products (TPs) were identified on the basis of molecular ions and mass fragment ions by MS spectrum during photocatalysis in the presence of 0.5 g L⁻¹ TiO₂ P-25 and UV-A. Information concerning the TPs is summarized in Table 2, while Fig. 8 shows the tentative transformation pathways of clopyralid, the products detected and the hypothetical intermediates within bracket (blue color). It has
Photocatalytic degradation of clopyralid: kinetics, degradation pathways and ecotoxicity

Table 2. LC-MS data of clopyralid and its detected transformation products during heterogeneous photocatalysis in the presence of 0.5 g L⁻¹ TiO₂ P25 and UV-A irradiation

<table>
<thead>
<tr>
<th>TPs</th>
<th>tₖ (min)</th>
<th>Elemental composition</th>
<th>Molecular ion (m/z)</th>
<th>Mass fragments [m/z] (% abundance)</th>
</tr>
</thead>
<tbody>
<tr>
<td>TP190</td>
<td>10.1</td>
<td>C₄ H₅ Cl NO₄</td>
<td>190</td>
<td>107(84.82), 110(20.24), 134(23.41), 146(23.24), 158(30.26), 162(24.30), 174.00(41.87), 190(100.00)</td>
</tr>
<tr>
<td>TP174A</td>
<td>11.2</td>
<td>C₆ H₄ Cl NO₃</td>
<td>174</td>
<td>110(9.03), 134(14.25), 158(13.20), 162(10.92), 174(100.00)</td>
</tr>
<tr>
<td>TP174B</td>
<td>12.4</td>
<td>C₆ H₄ Cl NO₃</td>
<td>174</td>
<td>107(20.28), 134(21.71), 158(31.35), 162(22.78), 174(100.00)</td>
</tr>
<tr>
<td>TP130A</td>
<td>20.2</td>
<td>C₆ H₄ Cl NO</td>
<td>130</td>
<td>79(28.27), 97(15.42), 130(100.00)</td>
</tr>
<tr>
<td>TP130B</td>
<td>21.4</td>
<td>C₆ H₄ Cl NO</td>
<td>130</td>
<td>79(28.27), 97(15.42), 130(100.00)</td>
</tr>
<tr>
<td>TP208A</td>
<td>25.7</td>
<td>C₆ H₅ O₃ N Cl₂</td>
<td>208</td>
<td>107(20.65), 134(22.76), 162(23.75), 174(100.00), 190(28.37), 208(51.19)</td>
</tr>
<tr>
<td>TP208B</td>
<td>28.4</td>
<td>C₆ H₅ O₃ N Cl₂</td>
<td>208</td>
<td>107(16.46), 134(18.81), 162(18.77), 174(77.58), 190(25.10), 208(100.00)</td>
</tr>
<tr>
<td>Clopyralid</td>
<td>29.6</td>
<td>C₆ H₄ O₂ N Cl₂</td>
<td>192</td>
<td>110(3.82), 146(4.84), 164(6.67), 174(11.04), 192(100.00), 208(9.97), 220(4.42), 256(4.41), 291(4.37), 319(4.53), 337(5.68), 338(4.58)</td>
</tr>
<tr>
<td>TP164</td>
<td>34.8</td>
<td>C₆ H₄ O N Cl₂</td>
<td>164</td>
<td>110(9.17), 146(10.84), 164(100.00)</td>
</tr>
<tr>
<td>TP220</td>
<td>48.7</td>
<td>-</td>
<td>220</td>
<td>110(17.17), 134(24.17), 162(24.13), 174(63.74), 192(27.17), 208(29.55), 220(100.00)</td>
</tr>
<tr>
<td>TP337</td>
<td>51.21</td>
<td>C₁₁ H₄ Cl₄ N₂ O₂</td>
<td>337</td>
<td>158(37.02), 220(60.11), 256(100.00), 291(46.17), 319(47.90), 337(71.76), 338(46.83)</td>
</tr>
</tbody>
</table>

![Figure 7](http://www.soci.org/)

Figure 7. Release of total inorganic nitrogen during photocatalytic mineralization of 40 mg L⁻¹ clopyralid, in the presence of 0.5 g L⁻¹ catalyst and UV-A irradiation: (●) TiO₂ P25, (●) TiO₂ P25 and 100 mg L⁻¹ H₂O₂, (●) TiO₂ UV-100, (●) TiO₂ UV-100 and 100 mg L⁻¹ H₂O₂.

been concluded that degradation of clopyralid is mainly initiated by pyridine ring transformation (Pathway 1, P1), dechlorination (Pathway 2, P2) and decarboxylation (Pathway 3, P3). In Pathway 1, TP207A and TP207B are both obtained from the hydroxylation at meta or para position of the pyridine ring. Further hydroxylation led to decarboxylation and opening of the pyridine ring. Pathway 2 results from the elimination of one chlorine atom by the clopyralid molecule, which leads to the formation of the two hydroxyl isomers, namely 6-chloro-3-hydroxypicolinic acid (TP174A) and 3-chloro-6-hydroxypicolinic acid (TP174B). Afterwards, these products undergo a series of hydroxylation and oxidation processes that substitute the next chlorine atom of the aromatic ring and generate the corresponding phenolic and keto products. The oxidative ring-opening reactions follow, to form the short-chain carboxylic acids and inorganic ions. In the third pathway, the parent molecule, upon the transfer of one electron can form a radical anion, which after decarboxylation and attack of the OH• leads to the formation of 3,6-dichloropyridin-2-ol (TP164). Successive •OH radical attack at halogenated and non-halogenated sites leads, ultimately, to hydroxy derivatives and/or keto intermediates and finally, to open-ring products. Finally, the last pathway involves the formation of the dimer derivative (3,3’,6,6’-tetrachloro-2,4’-bipyridine-2’-carboxylic acid, TP337), through the reaction of the intermediate radical species.

The reaction pathways proposed here, although with some similarities, differ from others previously reported in the literature. It has been reported that in electro-Fenton processes, clopyralid degradation occurs mainly due to the initial dechlorination and formation of hydroxy derivatives by the electrophilic substitution of the chlorine atoms in which the hydroxyl radicals causes an ipso-attack on C-carrying. In the TiO₂ photocatalytic treatment reported by Šojić et al., clopyralid showed similar, but not identical, reaction pathways with our study, leading to hydroxylated and decarboxylated intermediates and dimer products. However, formation of chloro-hydroxypicolinic acid derivatives, 5-chloropyridin-2-ol and 6-chloropyridin-3-ol, was not observed by Šojić et al.

For better knowledge of the photocatalytic process and assessment of the main transformation routes, an evaluation of the TPs generated during photocatalysis in the presence of 0.5 g L⁻¹ TiO₂ P25 and UV-A was carried out, as a function of the peak area obtained in the LC analysis. Typical bell-shaped profiles were obtained in most cases (Fig. 9). Compounds detected at higher concentration in this period were TP174A and TP164, suggesting that P2 and P3 are among the major pathways in the clopyralid degradation. The monochlorinated products, TP174A and TP174B, appear promptly; they reach a concentration maximum after 10 and 30 min, respectively, before being degraded in turn. By comparing the evolution profiles for these products it appears that the TP174A product at retention time (tₖ) 11.2 min is the most abundant, whereas the one at tₖ = 12.4 min is the least concentrated, indicating differences in ionization efficiency or a partially regioselective attack from the •OH radicals. The same observation applies to TP208 product, with the species at tₖ = 25.7 min (TP208A) being the most abundant compared with that at tₖ = 28.4 min (TP208B). After 30 min the concentration of all TP174 and TP208 isomers decreases forming second generation products. The rest of TPs were present at lower concentrations. After a tₖ = 120 min, most of the TPs were present at low concentrations. These data are in concordance with the fast accumulation rate of chloride ions (Fig. 6) and DOC values measured during the assays (Figs. 3 and 4).
**Acute toxicity evaluation**

An important goal of this study was to determine whether or not the TPs generated during the photocatalytic treatment present residual toxicity. Thus, acute toxicity of samples collected at various timepoints during photocatalysis in the presence of 0.5 g L\(^{-1}\) TiO\(_2\) P25 and UV-A was evaluated employing *V. fischeri* marine bacteria, by estimating the percentage of inhibition of each sample after 5, 15 and 30 min exposure of the bacteria to the photocatalytically treated samples (Fig. 10).

The untreated clopyralid solution (40 mg L\(^{-1}\)) was found to be very toxic to *V. fischeri* inducing an initial inhibition of 83% after 15 min incubation. The toxicity profile of the irradiated
mixtures showed an increasing trend of toxicity which could be attributed to the progressive formation of more toxic compounds than the parent herbicide, or to synergistic effects among the TPs. The highest toxicity (100% inhibition) was observed at irradiation times where the majority of the identified TPs attained almost their maximum concentration, suggesting that clopyralid and its TPs have high acute toxicity effects on the tested bacteria. Bioluminescence inhibition values remained stable at the initial stages of the transformation process between 10 and 60 min. Thereafter, inhibition of bioluminescence was progressively decreased (34% at 360 min), implying that total detoxification would be achieved at prolonged irradiation times. A similar trend in toxicity evaluation was also observed by Soils et al., who studied the TPs of clopyralid after ozonation treatment.36

CONCLUSIONS
Heterogenous photocatalytic degradation and mineralization of the herbicide clopyralid has been studied. Degradation follows pseudo-first-order kinetics, with TiO2 P25 providing the best results among the tested commercial TiO2. Catalyst’s loading, H2O2 concentration and pH affect the degradation kinetics. The initial degradation rate sharply increases with increasing TiO2 P25 loading, especially up to 1.0 g L−1, while addition of 100 mg L−1 H2O2 achieves maximum increase of the initial degradation rate. The most favorable pH for decomposition of the herbicide was 4.7, while both degradation and mineralization rates gradually decrease as photocatalysis takes place in neutral or alkaline pH values. Organic chlorine and nitrogen is easily converted into inorganic in the presence of 0.5 g L−1 TiO2 P25 presenting almost 90% conversion within 180 min illumination in both cases. Photocatalysis by TiO2 UV-100/UV-A, under the same experimental conditions, leads to lower conversion rates. In both cases the photocatalyst’s activity is enhanced in the presence of H2O2.

Degradation of clopyralid was mainly initiated by pyridine ring transformation, dechlorination, and decarboxylation reactions. The toxicity profile of the irradiated samples initially showed an increasing trend possibly due to the formation of toxic intermediates, or due to synergistic effects among them. Thereafter, eco-toxicity decreased implying that total detoxification would be achieved at prolonged irradiation times. These findings suggest that TiO2 mediated photocatalysis has the potential to provide a sustainable solution in the detoxification of wastewater containing recalcitrant pesticides, either alone or in combination with other methods, i.e. biological degradation in constructed wetlands, reducing the relevant environmental impact and creating water suitable for reuse applications (e.g. irrigation).

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